

## Corrosion Data

**Table 16-1 Dissociation constants of weak electrolytes at 35°C**

Reaction	K
$H_3BO_3 = H^+ + H_2BO_3^-$	$5.79 \times 10^{-7}$
$H_2CO_3 = H^+ + HCO_3^-$	$4.45 \times 10^{-7}$
$HCO_2^- = H^+ + CO_3^{--}$	$4.69 \times 10^{-11}$
$HCOOH = H^+ + HCOO^-$	$1.77 \times 10^{-4}$
$H_2C_2O_4 = H^+ + HC_2O_4^-$	$5.9 \times 10^{-2}$
$HC_2O_4^- = H^+ + C_2O_4^{--}$	$5.18 \times 10^{-5}$
$HCN = H^+ + CN^-$	$4 \times 10^{-10}$
$HClO = H^+ + ClO^-$	$5.6 \times 10^{-8}$
$HCrO_3^- = H^+ + CrO_4^{--}$	$3.2 \times 10^{-7}$
$Cr_2O_7^{--} + H_2O = 2HCrO_4^-$	$2.3 \times 10^{-2}$
$HNO_2 = H^+ + NO_2^-$	$4.5 \times 10^{-4}$

$NH_4OH = NH_4^+ + OH^-$	$1.81 \times 10^{-5}$
$H_2O = H^+ + OH^-$	$1.008 \times 10^{-14}$
$H_2O_2 = H^+ + HOO^-$	$2.4 \times 10^{-12}$
$H_3PO_4 = H^+ + H_2PO_4^-$	$7.52 \times 10^{-3}$
$H_2PO_4^- = H^+ + HPO_4^{--}$	$6.22 \times 10^{-3}$
$HPO_4^{--} = H^+ + PO_4^{---}$	$1 \times 10^{-12}$
$H_2SiO_3 = H^+ + HSiO_3^-$	$1 \times 10^{-10}$
$HSiO_3^- = H^+ + SiO_3^{--}$	$1 \times 10^{-11}$
$H_2S = H^+ + HS^-$	$1.15 \times 10^{-7}$
$HS^- = H^+ + S^{--}$	$1.0 \times 10^{-11}$
$H_2SO_3 = H^+ + HSO_3^-$	$1.72 \times 10^{-2}$
$HSO_3^- = H^+ + SO_3^{--}$	$6.24 \times 10^{-3}$
$HSO_4^- = H^+ + SO_4^{--}$	$1.01 \times 10^{-2}$
$CH_3COOH = H^+ + CH_3COO^-$	$1.76 \times 10^{-5}$

**Table 16-2 Dissociation constants of some weak electrolytes as a function of temperature**

Reaction	Experimental Temperature Range, °C	A	B	C
$H_3BO_3 = H^+ + H_2BO_3^-$	5 to 50	-2193.55	3.0395	-0.016499
$HCO_3^- = H^+ + CO_3^{--}$	0 to 50	-2902.39	6.4980	-0.02379
$HCOOH = H^+ + HCOO^-$	0 to 60	-1342.85	5.2744	-0.0151682
$HC_2O_4^- = H^+ + C_2O_4^{--}$	0 to 50	-1539.31	7.1966	-0.021200
$H_2O = H^+ + OH^-$	0 to 300	-4470.99	6.0875	-0.017060
$H_3PO_4 = H^+ + H_2PO_4^-$	0 to 50	-1264.51	7.6601	-0.018590
$H_2PO_4^- = H^+ + HPO_4^{--}$	5 to 50	-1648.88	3.2542	-0.016534
$CH_3COOH = H^+ + CH_3COO^-$	0 to 60	-1170.48	3.1649	-0.013399

The constants A, B, and C, on being inserted in the equation

$$\log_{10}K = \frac{A}{T} + B + CT$$

will give K as a function of T, where T = deg. Kelvin (deg. C + 273.1°). From H.S. Harned and B. B. Owen, *The Physical Chemistry of Electrolytic Solutions*, American Chemical Society Monograph 95, Reinhold Publishing Corp., New York, 1943.

t°C	$H_2CO_3 = H^+ + HCO_3^-$ K	$HSO_4^- = H^+ + SO_4^{--}$ K	t°C	$NH_4OH = OH^- + NH_4^+$ K
0	$2.647 \times 10^{-7}$	....	18	$1.72 \times 10^{-5}$
5	$3.040 \times 10^{-7}$	$1.80 \times 10^{-2}$	25	$1.81 \times 10^{-5}$
10	$3.430 \times 10^{-7}$	....	51	$1.81 \times 10^{-5}$
15	$3.802 \times 10^{-7}$	$1.36 \times 10^{-2}$	75.2	$1.64 \times 10^{-5}$
20	$4.147 \times 10^{-7}$	....	100	$1.35 \times 10^{-5}$
25	$4.452 \times 10^{-7}$	$1.01 \times 10^{-2}$	124.8	$1.04 \times 10^{-5}$
30	$4.710 \times 10^{-7}$	....	156	$0.63 \times 10^{-5}$
35	$4.914 \times 10^{-7}$	$0.75 \times 10^{-2}$	218	$0.18 \times 10^{-5}$
40	$5.058 \times 10^{-7}$	....	306	$0.0093 \times 10^{-5}$

45	$5.139 \times 10^{-7}$	$0.56 \times 10^{-2}$	
50	$5.161 \times 10^{-7}$	....	
55	....	$0.41 \times 10^{-2}$	

\* H.S. Harned and R. Davis, Jr., *J. Am. Chem. Soc.*, **65**, 2030 (1943).

† H.S. Harned and B.B.Owen, *The Physical Chemistry of Electrolytic Solutions*, American Chemical Society Monograph 95, Reinhold Publishing Corp., New York, 1943.

‡ A. Noyes and Y. Kato, *Carnegie Inst., Publ.* **63**, 178 (1907). R.B. Sosman, *op. cit.*, p. 228

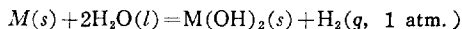
**Table 17. Spontaneity of common corrosion reactions\***

Metal	Solid Product <sup>†</sup>	Hydrogen-Type‡		Oxygen-Type§	
		Corrosion, p.H <sub>2</sub> =1.0atm. E (volt)	ΔF per gram atom Metal, gram cal	Corrosion, p <sup>o</sup> O <sub>2</sub> =0.21 atm. E (volt)	ΔF per gram atom Metal, gram cal
Mg	Mg(OH) <sub>2</sub>	+1.823	-84,000	+3.042	-140,000
Al	Al(OH) <sub>3</sub> (?)	+1.48	-102,600	+2.70	-180,700
Mn	Mn(OH) <sub>2</sub>	+0.60	-27,600	+1.81	-83,200
	Mn(OH) <sub>2</sub>	+0.256	-17,700	+1.50	-10,000
	MnO <sub>2</sub>	-0.14	+12,700	+1.11	-101,000
Cr	Cr(OH) <sub>3</sub>	+0.47	-32,500	+1.69	-117,000
Zn	Zn(OH) <sub>2</sub> (?)	+0.417	-19,200	+1.636	-75,200
Fe	Fe <sub>3</sub> O <sub>4</sub>	+0.082	-5,000	+1.30	-80,000
	Fe(OH) <sub>2</sub>	+0.049	-2,300	+1.27	-58,500
	Fe(OH) <sub>3</sub>	-0.07	+4,700	+1.15	-80,000
Cd	Cd(OH) <sub>2</sub>	-0.013	+600	+1.1206	-55.600
Co	Co(OH) <sub>2</sub>	-0.098	+4,500	+1.12	-51,700
Ni	Ni(OH) <sub>2</sub>	-0.17	+7,800	+1.05	-48,500
Pb	PbO(red)	-0.250	+11,500	+0.97	-44,600
Cu	Cu <sub>2</sub> O	-0.413	+9,500	+0.80	-18,600
	Cu(OH) <sub>2</sub>	-0.604	+27,800	+0.615	-28,300
	CuO	-0.537	+24,800	+0.680	-31,500
Hg	HgO	-0.926	+42,600	+0.293	-13,600
	Hg <sub>2</sub> O	-0.951	+21,970	+0.268	-6,200
Ag	Ag <sub>2</sub> O	-1.172	+27,000	+0.047	-1,100

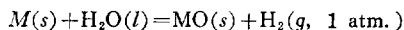
\* R. Brown, B. Roetheli, and H. Forrest, *Ind. Eng. Chem.*, **23**, 350 (1931) probably were the first investigators to attempt a summary of this type. They also used the terms *Hydrogen Type* and *Oxygen Type* in the same (cf. definitions below). For a more detailed discussion of these data, see J.C. Warner, *Trans. Electrochem. Soc.*, **83**, 319 (1943).

† Except when the formula is followed by(?), the data are quite certainly for the formation of the solid corrosion product as indicated. The formulas given do not, in any case, attempt to indicate the extent of hydration of the solid phase.

‡ The data in the column under "Hydrogen-Type Corrosion" are for reactions of the type

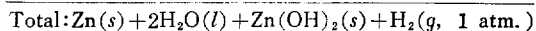
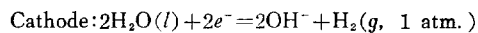
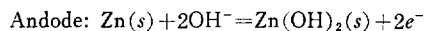


or



where *s*=solid, *l*=liquid, and *g*=gas.

The potentials given are the reversible potentials for the galvanic corrosion cells, in which the anode and cathode reactions add up to the overall corrosion reactions, thus:

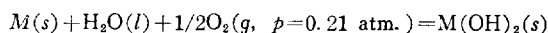


A positive value for  $E$  or a negative value for  $\Delta F$  corresponds to a spontaneous reaction. This follows the convention

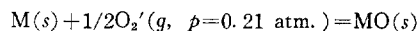
$$\Delta F = -nFE$$

where  $F$ =Faraday (96, 501 coulombs),  $E$ =emf, and  $n$ =number of electrons (equivalents) taking part in the reaction.

§ In the columns under "Oxygen-Type Corrosion" the data are for reactions of the type



or



The data have been calculated for these reactions with  $\text{O}_2$  at a partial pressure of 0.21 atmosphere because this is approximately the partial pressure of  $\text{O}_2$  in dry air under a total pressure of one atmosphere.

**Table 18. Galvanic Series for High Purity Metals (69 Days in Sea Water at Key West, Florida)**

Metal	Metal Purity (%)	Median Potential (Volts) SCE Reference
(Cathodic)		
Palladium	99.99+	+0.308
Platinum	99.99+	+0.295
Titanium	Iodide(zone refined)	+0.200
Tantalum	99.9	+0.195
Gold	99.97+	+0.175
Columbium	99.9	+0.110
(Niobium)		
Zirconium	99.9	+0.010
Silver	99.95	-0.025
Nickel	99.99+(zoner refined)	-0.038
Siver	99.999	-0.115
Copper	99.99+(zone refined)	-0.141
Nickel	99.99-(zone refined)	-0.172
Tantalum	99.99-(zone refined)	-0.172
Molybdenum	99.9	-0.173
Vanadium	99.99+(zone refined)	-0.209
Tungsten	99.9	-0.240
Bismuth	99.9	-0.248
Indium	99.999(spectrographic grade)	-0.368
	Rerun	-0.525
Tin	99.999(spectrographic grade)	-0.671
Iron	99.9-(electrolytic grade)	-0.749
Alumium	99.99+(zone refined)	-1.472
(Anodic)	99.99+(ingot)	-1.455

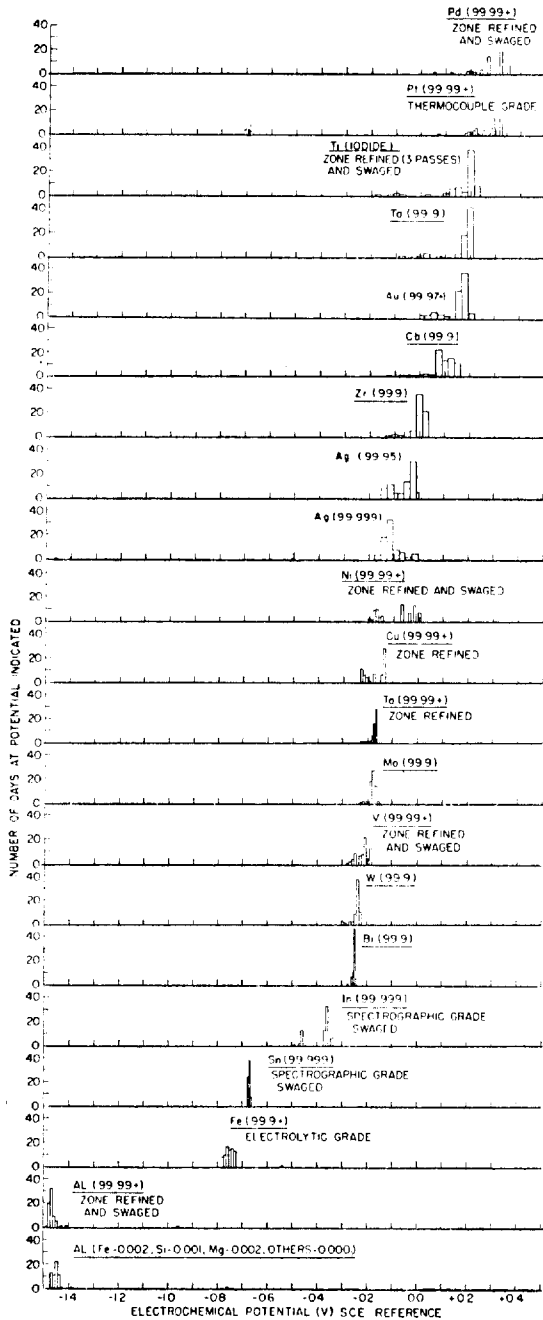


Fig. 1 Histograms of the electrochemical potentials for high purity metals exposed 69 days in quiescent sea water at Keywest, Florida

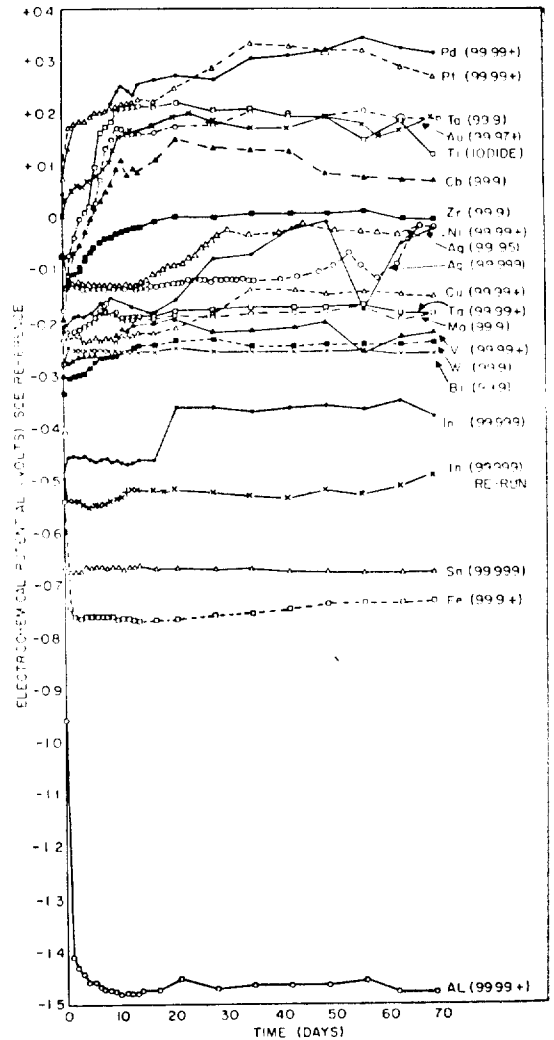


Fig. 2 Electrochemical potentials vs time graphs for high purity metals exposed 69 days in quiescent sea water at key west, Florida

**Table. 19-1 Paints used for atmospheric tests The paint code names are also used for immersion and other tests**

Priming paints

Code	Description
UNMOD PTP	Pretreatment primer (unmodified), to 'Bakelite' formula W.P.I.
MOD PTP	Pretreatment primer (modified), to the 'Bakelite' modification of formula W.P.I.
ZN CHROME	Zinc chromate in a linseed in a linseed-tung phenolic medium, to D.E.F. specification No. 1039
CA PLUMBATE	Calcium plumbate in oil to B.S. 3698: 1964 Type A
CL RUBBER	Chlorinated rubber sealer (unpigmented)
RED OXIDE	Red oxide in oil, to B.S. 2524: 1954
AL BITUMEN	Aluminium in a blown bitumen solution
RED LEAD A	Red lead in oil to B.S. 2523: 1594 Type A
ZN RICH EPOXIDE	Zinc-rich in an epoxy-polyamide medium, to the 'Shell' formula. TB/RES/154/1

Finishing paints

Code	Description
MIO	Micaceous iron oxide in a long-oil tungphenolic medium, to B.T.C. Specification No. 35, items 61, 62 and 63
RT ALKYD	Rutile titanium dioxide in a long-oil alkyd medium, to D.E.F. 1156
AL BITUMEN	Aluminium in bitumen (as primer above)
AL TUNG	Aluminium in a tung-phenolic medium to C.S. 2686
C-T EPOXIDE	Coal-tar epoxide paint No. 834 to the 'Shell' formula TB/RES/136/1

**Table 19-2 Condition after 5 years' exposure of the painted bare steel specimens in the atmosphere**

- |   |                             |
|---|-----------------------------|
| Condition of paint                        | Cause of failure            |
| A In good condition                       | (R) Rust                    |
| B Beginning to fail (should be repainted) | (E) Chalking and/or erosion |
| C Overdue for repainting                  |                             |
| D Failed (some loss of basis steel)       |                             |

Paint scheme (for paint code see <b>Table 1</b> )	tatford	Shoreham	Osu*
	Industrial	Industrial/marine	Tropical/surf
A15 UNMOD PTP, ZN CHROME, 2 coats MIO	A A	C(R) B(R)	C(R) C(R)
A19 2 coats RED LEAD A, 2 coats RT ALKYD	A A	B(R) C(R)	D(R) D(R)
A20 ZN RICH EPOXIDE, 2 coats C-T EPOXIDE	A A	B(R) B(R)	C(R) C(R)

Note: A20 is identical with S11

\*4½ years' exposure at Osu



Table 19-4 Condition after 5 years' immersion of paint schemes applied over sprayed metal coatings

Condition of paint  
 A In good condition  
 B Beginning to fail(should be repainted)  
 C Overdue for repainting  
 D Failed(some loss of basis steel)

Cause of failure  
 Bl Blisters  
 Cr Cracking  
 Cp Corrosion product  
 E Erosion  
 Fl Flaking

Paint scheme (for paint code see Table 1)	'Normal' schemes				Variants						
	Brighton Pier		Avon Dam		Brighton Pier		Avon Dam		Weathered for 6 months after priming		
	Half-tide immersion	Full immersion	Half-tide immersion	Full immersion	Half-tide immersion	Full immersion	Half-tide immersion	Full immersion	Half-tide immersion	Full immersion	
S1	CL RUBBER—3 coats chlorinated rubber	Al	Zn Alloy	Al	Zn Alloy	Al	Zn	Al	Zn	Al	Zn
S2	MOD PTP—3 coats chlorinated rubber	BCp		A	A						
S3	3 coats aluminium/vinyl-copolymer	A		A							
S4	MOD PTP—3 coats aluminium/vinyl-copolymer	A	A BFl	A	A	A	A	A	A	A	A
S5	ZN CHROME—2 coats MIO	CFI	BCp								
S6	MOD PTP—ZN CHROME—2 coats MIO	A	CFI								
S7	MOD PTP—ZN CHROME—2 coats micaceous iron oxide/polyurethane	A	CFI	A	A	A	A	A	A	CBI	CBI
S8	3 coats AL TUNG	A		A							
S9	3 coats AL BITUMEN	A	BCp	A	A	A	A	A	A		
S10	MOD PTP—3 coats BISRA paint No. 655	C E	C E			C E	C E	C E	C E	C E	C E
S13	2 coats C-T EPOXIDE	A	BBI BFl			CFI	CFI				

Notes: The chlorinated rubber systems in S1, S2 and S12(Table 24) were the same  
 The aluminium/vinyl copolymer systems in S3 & S4 were the same  
 BISRA 655 (in S10) is aluminium/basic lead sulphate/iron oxide in a linseed-tung-phenolic medium

**Table 19-5 Condition after 5 years' exposure of the painted bare steel specimens in the immersion test**

- |   |                             |
|---|-----------------------------|
| Condition of paint                        | Cause of failure            |
| A In good condition                       | (R) Rust                    |
| B Beginning to fail (should be repainted) | (E) Chalking and/or erosion |
| C Overdue for repainting                  |                             |
| D Failed (some loss of basis steel)       |                             |

Paint scheme (for paint code sec <b>Table 1</b> )	Brighton Pier	Avon Dam
	Half-tide immersion	Full immersion
MOD PTP, 3 coats BISRA 655	C(E)	A
S11 ZN RICH EPOXIDE, 2 coats C-T EPOXIDE  4-coat chlorinated rubber system (primer zinc-rich)	—	A
	A	A
	—	A
	A	A
	—	A

**Table 19-6 Condition after 5 years of the metal coatings bare at all sites**

- |                                     |                  |
|-------------------------------------|------------------|
| Condition of coating                | Cause of failure |
| A In good condition                 | (R) Rust         |
| B Beginning to fail                 |                  |
| D Failed (Some loss of basis steel) |                  |

Metal coating, 4 mil minimum (100 microns)	Stratford	shoreham	Osu*	Brighton Pier	Avon Dam
	industrial	Industrial/ marinc	Tropical/surf	Half-tide immersion	Full immersion
Aluminium	A	A	A	B	A
	A	A	A	—	A
	A	A	D(R)	D(R)	D(R)
	A	A	D(R)	—	D(R)
Zinc/aluminium alloy	A	A	—	—	—
	A	A	—	—	—

\*4½ years' exposure at Osu